

**DuPont™**  
refrigerants

**Thermodynamic  
Properties  
of**

**DuPont™  
Freon® 22**

**Refrigerant**

**(Chlorodifluoromethane)**

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*The miracles of science™*



# PHYSICAL PROPERTIES

Chemical Formula:	CHClF <sub>2</sub>	Viscosity, $\eta$ , in Centipoises:	
Molecular Weight:	86.476	<u>t °F</u>	<u><math>\eta</math></u>
Boiling Point at one atmosphere, °F	-41.36	Liquid	
Freezing Point, °F	-256	-40	0.349
Critical Temperature, °F	204.81	0	0.298
Critical Pressure, psia	721.906	40	0.261
Critical Density, lb/cu ft	32.76	120	0.211
Critical Volume, cu ft/lb	0.030525	Vapor (one atmosphere)	
Refractive Index ( $n_D$ ), 70°F		-40	0.0100
Liquid	1.259	0	0.0111
Vapor (one atmosphere)	1.00073	40	0.0121
Dielectric Constant:		120	0.0140
Liquid at 75°F	6.11	Surface Tension, $\gamma$ , in dynes/cm:	
Vapor (0.5 atmosphere) at 78°F	1.0035	<u>t °F</u>	<u><math>\gamma</math></u>
Relative Dielectric Strength ( $N_2 = 1$ )	1.3	-40	18.5
at 1 atmosphere with 0.1-inch gap		0	14.9
and 0.75-inch-sphere-to-plane gap		40	11.4
at 77°F.		120	4.9
Thermal Conductivity, $k$ , in		Solubility of Water in the Liquid:	
Btu/(hr)(ft)(°F)		<u>t °F</u>	<u>ppm</u>
<u>t °F</u>	<u><math>k</math></u>	-100	19
Liquid		-40	120
-40	0.0792	40	690
0	0.0698	100	1800
40	0.0605		
120	0.0417		
Vapor (one atmosphere)			
-40	0.0050		
0	0.0056		
40	0.0061		
120	0.0072		

## UNITS AND FACTORS

<p><math>t</math> = temperature in °F  <math>T</math> = temperature in °R = °F + 459.69            psia = pressure in lb/sq in absolute            psig = pressure in lb/sq in gage  <math>p</math> = pressure of vapor in psia  <math>p_{sat}</math> = pressure of saturated vapor in psia  <math>v_f</math> = volume of the saturated liquid in cu ft/lb  <math>v_g</math> = volume of the saturated vapor in cu ft/lb  <math>V</math> = volume of the superheated vapor in cu ft/lb  <math>d_f = 1/v_f</math> = density of the saturated liquid in lb/cu ft  <math>d_g = 1/v_g</math> = density of the saturated vapor in lb/cu ft  <math>h_f</math> = enthalpy of the saturated liquid in Btu/lb  <math>h_{fg}</math> = enthalpy of vaporization in Btu/lb  <math>h_g</math> = enthalpy of the saturated vapor in Btu/lb  <math>H</math> = enthalpy of the superheated vapor in Btu/lb</p>	<p><math>s_f</math> = entropy of the saturated liquid in Btu/(lb)(°R)  <math>s_g</math> = entropy of the saturated vapor in Btu/(lb)(°R)  <math>S</math> = entropy of the superheated vapor in Btu/(lb)(°R)  <math>c_f</math> = heat capacity of the saturated liquid in Btu/(lb)(°F)  <math>c_v^o</math> = heat capacity of the vapor at constant volume in Btu/(lb)(°F) at zero pressure  <math>c_p</math> = heat capacity of the vapor at constant pressure in Btu/(lb)(°F)  <math>c_v</math> = heat capacity of the vapor at constant volume in Btu/(lb)(°F)  <math>k</math> = thermal conductivity in Btu/(hr) (ft) (°F)  <math>\eta</math> = viscosity in centipoises  <math>\gamma</math> = surface tension in dynes/cm  <math>n_D</math> = refractive index  <math>e</math> = base of natural logarithms = 2.718281828</p>
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The gas constant,  $R = 10.7315$  (psia) (cu ft)/(°R) (lb mol)  
 Heat units (Btu/lb) = work units (psia) (cu ft/lb)  $\times 0.185053$   
 One atmosphere = 14.696 psia = 29.9212 inches of mercury

## EQUATIONS

The four basic equations used to calculate the tables of thermodynamic properties are given below. They were developed by Prof. J. J. Martin at the University of Michigan. Programming and computations were also carried out at the University under his supervision.

### 1. Vapor Pressure

$$\log_{10} P_{sat} = A - \frac{B}{T} - C \log_{10} T + DT + \frac{E(F-T)}{FT} \log_{10}(F-T)$$

$$\begin{aligned} A &= 29.35754453 & D &= 0.002190939044 \\ B &= 3845.193152 & E &= 305.8268131 \\ C &= 7.86103122 & F &= 686.1 \end{aligned}$$

Range of Data: 0.08 psia to 692 psia.

Average Deviation: 0.11%.

Based on data from Prof. A. Michels at the University of Amsterdam and checked with data from the University of Michigan and the Du Pont Company.

### 2. Equation of State

$$p = \frac{RT}{V-b} + \frac{A_2 + B_2T + C_2e^{kT/Tc}}{(V-b)^2} + \frac{A_3 + B_3T + C_3e^{kT/Tc}}{(V-b)^3} + \frac{A_4 + B_4T}{(V-b)^4} + \frac{A_5 + B_5T + C_5e^{kT/Tc}}{(V-b)^5} + \frac{A_6 + B_6T}{e^{548.2V}}$$

$$\begin{aligned} R &= 0.124098 & A_4 &= 0.002310142 \\ b &= 0.002 & B_4 &= -3.605723 \times 10^{-6} \\ A_2 &= -4.353547 & A_5 &= -3.724044 \times 10^{-5} \\ B_2 &= 0.002407252 & B_5 &= 5.355465 \times 10^{-8} \\ C_2 &= -44.066868 & C_5 &= -1.845051 \times 10^{-4} \\ A_3 &= -0.017464 & A_6 &= 1.363387 \times 10^8 \\ B_3 &= 7.62789 \times 10^{-5} & B_6 &= -1.672612 \times 10^5 \\ C_3 &= 1.483763 & k &= -4.2 \end{aligned}$$

Range of Data: Vapor densities from 1.6 to 42 lb/cu ft.  
Average Deviation: 0.07%

Based on data from Prof. A. Michels at the University of Amsterdam and checked with data from the University of Michigan and the Du Pont Company.

### 3. Density of the Saturated Liquid

$$d_f = A + B \left(1 - \frac{T}{T_c}\right)^{1/3} + C \left(1 - \frac{T}{T_c}\right)^{2/3} + D \left(1 - \frac{T}{T_c}\right) + E \left(1 - \frac{T}{T_c}\right)^{4/3}$$

$$\begin{aligned} A &= 32.76 & D &= -22.2925657 \\ B &= 54.6344093 & E &= 20.47328862 \\ C &= 36.74892 \end{aligned}$$

Range of Data: 100 lb/cu ft to 51 lb/cu ft

Average Deviation: 0.08%

### 4. Heat Capacity of the Vapor

$$c_v^o = a + \frac{b}{T^2} + cT + dT^2$$

$$\begin{aligned} a &= 2.812836 \times 10^{-2} \\ b &= 257.341 \\ c &= 2.255408 \times 10^{-4} \\ d &= -6.509607 \times 10^{-8} \end{aligned}$$

Range of Data: -280°F to 530°F (calculated from spectroscopic data)

Average Deviation: 0.07%

TABLE I HCFC-22 SATURATION PROPERTIES-TEMPERATURE TABLE

Table with columns: TEMP. °F, PRESSURE (PSIA, PSIG), VOLUME (LIQUID v\_f, VAPOR v\_g) cu ft/lb, DENSITY (LIQUID l/v\_f, VAPOR l/v\_g) lb/cu ft, ENTHALPY (LIQUID h\_f, LATENT h\_fg, VAPOR h\_g) Btu/lb, ENTROPY (LIQUID s\_f, VAPOR s\_g) Btu/(lb)(°R), TEMP. °F.

\*Inches of mercury below one atmosphere









TABLE I "FREON" 22 SATURATION PROPERTIES—TEMPERATURE TABLE

TEMP. °F	PRESSURE		VOLUME cu ft/lb		DENSITY lb/cu ft		ENTHALPY Btu/lb			ENTROPY Btu/(lb(°R))		TEMP. °F
	PSIA	PSIG	LIQUID <i>v<sub>f</sub></i>	VAPOR <i>v<sub>g</sub></i>	LIQUID <i>l/v<sub>f</sub></i>	VAPOR <i>l/v<sub>g</sub></i>	LIQUID <i>h<sub>f</sub></i>	LATENT <i>h<sub>fg</sub></i>	VAPOR <i>h<sub>g</sub></i>	LIQUID <i>s<sub>f</sub></i>	VAPOR <i>s<sub>g</sub></i>	
65	125.93	111.23	0.013136	0.43663	76.126	2.2903	28.638	81.432	110.070	0.06021	0.21541	65
66	127.92	113.22	0.013159	0.42981	75.996	2.3266	28.932	81.208	110.140	0.06076	0.21524	66
67	129.94	115.24	0.013181	0.42311	75.865	2.3635	29.228	80.982	110.209	0.06131	0.21507	67
68	131.97	117.28	0.013204	0.41653	75.733	2.4008	29.523	80.755	110.278	0.06186	0.21490	68
69	134.04	119.34	0.013227	0.41007	75.601	2.4386	29.819	80.527	110.346	0.06241	0.21473	69
70	136.12	121.43	0.013251	0.40373	75.469	2.4769	30.116	80.298	110.414	0.06296	0.21456	70
71	138.23	123.54	0.013274	0.39751	75.336	2.5157	30.413	80.068	110.480	0.06351	0.21439	71
72	140.37	125.67	0.013297	0.39139	75.202	2.5550	30.710	79.836	110.547	0.06406	0.21422	72
73	142.52	127.83	0.013321	0.38539	75.068	2.5948	31.008	79.604	110.612	0.06461	0.21405	73
74	144.71	130.01	0.013345	0.37949	74.934	2.6351	31.307	79.370	110.677	0.06516	0.21388	74
75	146.91	132.22	0.013369	0.37369	74.799	2.6760	31.606	79.135	110.741	0.06571	0.21372	75
76	149.15	134.45	0.013393	0.36800	74.664	2.7174	31.906	78.899	110.805	0.06626	0.21355	76
77	151.40	136.71	0.013418	0.36241	74.528	2.7593	32.206	78.662	110.868	0.06681	0.21338	77
78	153.69	138.99	0.013442	0.35691	74.391	2.8018	32.506	78.423	110.930	0.06736	0.21321	78
79	155.99	141.30	0.013467	0.35151	74.254	2.8449	32.808	78.184	110.991	0.06791	0.21305	79
80	158.33	143.63	0.013492	0.34621	74.116	2.8885	33.109	77.943	111.052	0.06846	0.21288	80
81	160.68	145.99	0.013518	0.34099	73.978	2.9326	33.412	77.701	111.112	0.06901	0.21271	81
82	163.07	148.37	0.013543	0.33587	73.839	2.9774	33.714	77.457	111.171	0.06956	0.21255	82
83	165.48	150.78	0.013569	0.33083	73.700	3.0227	34.018	77.212	111.230	0.07011	0.21238	83
84	167.92	153.22	0.013594	0.32588	73.560	3.0686	34.322	76.966	111.288	0.07065	0.21222	84
85	170.38	155.68	0.013620	0.32101	73.420	3.1151	34.626	76.719	111.345	0.07120	0.21205	85
86	172.87	158.17	0.013647	0.31623	73.278	3.1622	34.931	76.470	111.401	0.07175	0.21188	86
87	175.38	160.69	0.013673	0.31153	73.137	3.2100	35.237	76.220	111.457	0.07230	0.21172	87
88	177.93	163.23	0.013700	0.30690	72.994	3.2583	35.543	75.968	111.512	0.07285	0.21155	88
89	180.50	165.80	0.013727	0.30236	72.851	3.3073	35.850	75.716	111.566	0.07339	0.21139	89
90	183.09	168.40	0.013754	0.29789	72.708	3.3570	36.158	75.461	111.619	0.07394	0.21122	90
91	185.72	171.02	0.013781	0.29349	72.564	3.4073	36.466	75.206	111.671	0.07449	0.21106	91
92	188.37	173.67	0.013809	0.28917	72.419	3.4582	36.774	74.949	111.723	0.07504	0.21089	92
93	191.05	176.35	0.013836	0.28491	72.273	3.5098	37.084	74.690	111.774	0.07559	0.21072	93
94	193.76	179.06	0.013864	0.28073	72.127	3.5621	37.394	74.430	111.824	0.07613	0.21056	94
95	196.50	181.80	0.013893	0.27662	71.980	3.6151	37.704	74.168	111.873	0.07668	0.21039	95
96	199.26	184.56	0.013921	0.27257	71.833	3.6688	38.016	73.905	111.921	0.07723	0.21023	96
97	202.05	187.36	0.013950	0.26859	71.685	3.7232	38.328	73.641	111.968	0.07778	0.21006	97
98	204.87	190.18	0.013979	0.26467	71.536	3.7783	38.640	73.375	112.015	0.07832	0.20989	98
99	207.72	193.03	0.014008	0.26081	71.386	3.8341	38.953	73.107	112.060	0.07887	0.20973	99
100	210.60	195.91	0.014038	0.25702	71.236	3.8907	39.267	72.838	112.105	0.07942	0.20956	100
101	213.51	198.82	0.014068	0.25329	71.084	3.9481	39.582	72.567	112.149	0.07997	0.20939	101
102	216.45	201.76	0.014098	0.24962	70.933	4.0062	39.897	72.294	112.192	0.08052	0.20923	102
103	219.42	204.72	0.014128	0.24600	70.780	4.0651	40.213	72.020	112.233	0.08107	0.20906	103
104	222.42	207.72	0.014159	0.24244	70.626	4.1247	40.530	71.744	112.274	0.08161	0.20889	104
105	225.45	210.75	0.014190	0.23894	70.472	4.1852	40.847	71.467	112.314	0.08216	0.20872	105
106	228.50	213.81	0.014221	0.23549	70.317	4.2465	41.166	71.187	112.353	0.08271	0.20855	106
107	231.59	216.90	0.014253	0.23209	70.161	4.3086	41.485	70.906	112.391	0.08326	0.20838	107
108	234.71	220.02	0.014285	0.22875	70.005	4.3715	41.804	70.623	112.427	0.08381	0.20821	108
109	237.86	223.17	0.014317	0.22546	69.847	4.4354	42.125	70.338	112.463	0.08436	0.20804	109
110	241.04	226.35	0.014350	0.22222	69.689	4.5000	42.446	70.052	112.498	0.08491	0.20787	110
111	244.25	229.56	0.014382	0.21903	69.529	4.5656	42.768	69.763	112.531	0.08546	0.20770	111
112	247.50	232.80	0.014416	0.21589	69.369	4.6321	43.091	69.473	112.564	0.08601	0.20753	112
113	250.77	236.08	0.014449	0.21279	69.208	4.6994	43.415	69.180	112.595	0.08656	0.20736	113
114	254.08	239.38	0.014483	0.20974	69.046	4.7677	43.739	68.886	112.626	0.08711	0.20718	114
115	257.42	242.72	0.014517	0.20674	68.883	4.8370	44.065	68.590	112.655	0.08766	0.20701	115
116	260.79	246.10	0.014552	0.20378	68.719	4.9072	44.391	68.291	112.682	0.08821	0.20684	116
117	264.20	249.50	0.014587	0.20087	68.554	4.9784	44.718	67.991	112.709	0.08876	0.20666	117
118	267.63	252.94	0.014622	0.19800	68.388	5.0506	45.046	67.688	112.735	0.08932	0.20649	118
119	271.10	256.41	0.014658	0.19517	68.221	5.1238	45.375	67.384	112.759	0.08987	0.20631	119



TABLE I HCFC-22 SATURATION PROPERTIES—TEMPERATURE TABLE

TEMP. °F	PRESSURE		VOLUME cu ft/lb		DENSITY lb/cu ft		ENTHALPY Btu/lb			ENTROPY Btu/(lb)(°R)		TEMP. °F
	PSIA	PSIG	LIQUID $v_f$	VAPOR $v_g$	LIQUID $l/v_f$	VAPOR $l/v_g$	LIQUID $h_f$	LATENT $h_{fg}$	VAPOR $h_g$	LIQUID $s_f$	VAPOR $s_g$	
175	525.39	510.70	0.017813	0.083914	56.139	11.917	66.194	44.644	110.838	0.12289	0.19323	175
176	531.17	516.47	0.017910	0.082473	55.834	12.125	66.643	44.056	110.699	0.12356	0.19287	176
177	537.00	522.30	0.018011	0.081040	55.523	12.340	67.098	43.455	110.553	0.12425	0.19250	177
178	542.87	528.18	0.018114	0.079616	55.205	12.560	67.558	42.841	110.400	0.12494	0.19212	178
179	548.80	534.11	0.018221	0.078200	54.881	12.788	68.025	42.213	110.238	0.12564	0.19173	179
180	554.78	540.09	0.018332	0.076790	54.549	13.023	68.498	41.570	110.068	0.12635	0.19133	180
181	560.82	546.12	0.018447	0.075386	54.209	13.265	68.978	40.911	109.888	0.12707	0.19092	181
182	566.90	552.21	0.018566	0.073987	53.861	13.516	69.465	40.235	109.700	0.12779	0.19050	182
183	573.04	558.35	0.018690	0.072592	53.503	13.776	69.960	39.540	109.500	0.12853	0.19005	183
184	579.24	564.54	0.018820	0.071201	53.136	14.045	70.464	38.826	109.290	0.12928	0.18960	184
185	585.49	570.79	0.018954	0.069811	52.759	14.324	70.977	38.090	109.067	0.13004	0.18913	185
186	591.80	577.10	0.019095	0.068421	52.370	14.615	71.500	37.332	108.832	0.13082	0.18864	186
187	598.16	583.46	0.019243	0.067031	51.968	14.918	72.034	36.548	108.582	0.13161	0.18813	187
188	604.58	589.88	0.019397	0.065638	51.553	15.235	72.579	35.738	108.317	0.13242	0.18760	188
189	611.05	596.36	0.019561	0.064241	51.123	15.566	73.138	34.897	108.035	0.13325	0.18704	189
190	617.59	602.89	0.019733	0.062837	50.677	15.914	73.711	34.023	107.734	0.13409	0.18646	190
191	624.19	609.49	0.019915	0.061424	50.213	16.280	74.300	33.112	107.412	0.13496	0.18585	191
192	630.84	616.14	0.020110	0.059999	49.728	16.667	74.907	32.160	107.067	0.13585	0.18520	192
193	637.56	622.86	0.020317	0.058558	49.219	17.077	75.534	31.162	106.696	0.13678	0.18452	193
194	644.33	629.64	0.020540	0.057096	48.685	17.514	76.184	30.111	106.295	0.13773	0.18380	194
195	651.18	636.48	0.020782	0.055609	48.119	17.983	76.861	28.998	105.858	0.13873	0.18302	195
196	658.08	643.38	0.021045	0.054089	47.518	18.488	77.568	27.813	105.381	0.13977	0.18218	196
197	665.05	650.35	0.021334	0.052528	46.874	19.038	78.313	26.543	104.856	0.14086	0.18128	197
198	672.08	657.39	0.021655	0.050912	46.178	19.642	79.102	25.169	104.270	0.14202	0.18029	198
199	679.19	664.49	0.022018	0.049224	45.417	20.315	79.946	23.664	103.610	0.14326	0.17918	199
200	686.36	671.66	0.022436	0.047438	44.571	21.080	80.862	21.990	102.853	0.14460	0.17794	200
201	693.60	678.90	0.022931	0.045513	43.609	21.972	81.875	20.086	101.961	0.14609	0.17649	201
202	700.91	686.21	0.023543	0.043375	42.476	23.055	83.030	17.840	100.870	0.14779	0.17475	202
203	708.29	693.59	0.024358	0.040868	41.054	24.469	84.418	15.022	99.439	0.14984	0.17250	203
204	715.75	701.05	0.025647	0.037545	38.991	26.635	86.309	10.951	97.260	0.15264	0.16914	204
204.81	721.91	707.21	0.030525	0.030525	32.760	32.760	91.329	0.000	91.329	0.16016	0.16016	204.81

TABLE II HCFC-22 SUPERHEATED VAPOR-CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

ABSOLUTE PRESSURE, lb/sq in

Table with columns for temperature (TEMP. °F) and absolute pressure (0.20, 0.25, 0.30, 0.35, 0.40, 0.45, 0.50, 0.60) and rows for values of V, H, and S. Includes saturation properties in parentheses.

\*Inches of mercury below one atmosphere



TABLE II HCFC-22 SUPERHEATED VAPOR-CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

Main data table with columns for Temperature (TEMP.) in °F and Absolute Pressure in lb/sq in (2.0, 2.5, 3.0, 3.5, 4.0, 4.5, 5.0, 5.5). Rows show values for Volume (V), Enthalpy (H), and Entropy (S) at various temperatures. The table is divided into two sections: one for pressures up to 3.5 lb/sq in and another for pressures up to 5.5 lb/sq in. Each pressure column has three sub-columns for V, H, and S, with saturation values in parentheses. The temperature range is from -100°F to 240°F.

\*Inches of mercury below one atmosphere

TABLE II HCFC-22 SUPERHEATED VAPOR—CONSTANT PRESSURE TABLES  
AT PRESSURE INTERVALS

V = volume in cu ft/lb; H = enthalpy in Btu/lb; S = entropy in Btu/(lb)(°R) (saturation properties in parentheses)

ABSOLUTE PRESSURE, lb/sq in

Table with columns for Absolute Pressure (6.0, 6.5, 7.0, 7.5, 8.0, 8.5, 9.0, 9.5) and rows for Temperature (°F). Each pressure column contains sub-columns for Volume (V), Enthalpy (H), and Entropy (S). Values include saturation points in parentheses and various thermodynamic data points.

\*Inches of mercury below one atmosphere





TABLE II HCFC-22 SUPERHEATED VAPOR-CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Bru/(lb)(°R) (saturation properties in parentheses)

Table with columns for TEMP. (°F), ABSOLUTE PRESSURE (lb/sq in) (15, 16, 17, 18), and TEMP. (°F). It contains thermodynamic data for HCFC-22 at various pressures and temperatures.











TABLE II HCFC-22 SUPERHEATED VAPOR-CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

ABSOLUTE PRESSURE, lb/sq in

Main data table with columns for Temperature (TEMP. °F) and Absolute Pressure (63, 64, 65, 66, 67, 68, 69, 70 lb/sq in). Each pressure column contains sub-columns for Volume (V), Enthalpy (H), and Entropy (S). Values include saturation properties in parentheses.









TABLE II HCFC-22 SUPERHEATED VAPOR-CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

Table with columns for Absolute Pressure (95, 96, 97, 98, 99, 100, 101, 102 lb/sq in) and Temperature (50-350 °F). Rows contain V, H, and S values for each pressure interval.





TABLE II HCFC-22 SUPERHEATED VAPOR—CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

Table with columns for Absolute Pressure (126, 128, 130, 132, 134, 136, 138, 140) and Temperature (°F). Each pressure column contains sub-columns for Volume (V), Enthalpy (H), and Entropy (S). Values are provided for temperatures from 70°F to 380°F.

















TABLE II "FREON" 22 SUPERHEATED VAPOR—CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

ABSOLUTE PRESSURE, lb/sq in

Table with columns for Temperature (TEMP. °F) and Absolute Pressure (254, 256, 258, 260, 262, 264, 266, 268). Each pressure column contains sub-columns for Volume (V), Enthalpy (H), and Entropy (S). The table lists values for temperatures from 120 to 420 degrees Fahrenheit.

TABLE II HCFC-22 SUPERHEATED VAPOR—CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft. lb.; H=enthalpy in Btu/lb.; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

Table with columns for Temperature (TEMP. °F) and Absolute Pressure (lb/sq in) intervals (270, 272, 274, 276, 278, 280, 282, 284). Each interval has sub-columns for Volume (V), Enthalpy (H), and Entropy (S). Values are listed for temperatures from 120 to 430 °F. Saturation properties are indicated by dashes in some cells.















TABLE II HCFC-22 SUPERHEATED VAPOR-CONSTANT PRESSURE TABLES AT PRESSURE INTERVALS

V=volume in cu ft/lb; H=enthalpy in Btu/lb; S=entropy in Btu/(lb)(°R) (saturation properties in parentheses)

Table with 14 columns and 48 rows for absolute pressures 505, 510, 515, and 520 lb/sq in. Includes sub-tables for pressures 525, 530, 535, and 540 lb/sq in. Columns include TEMP. °F, V, H, S, and TEMP. °F.



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